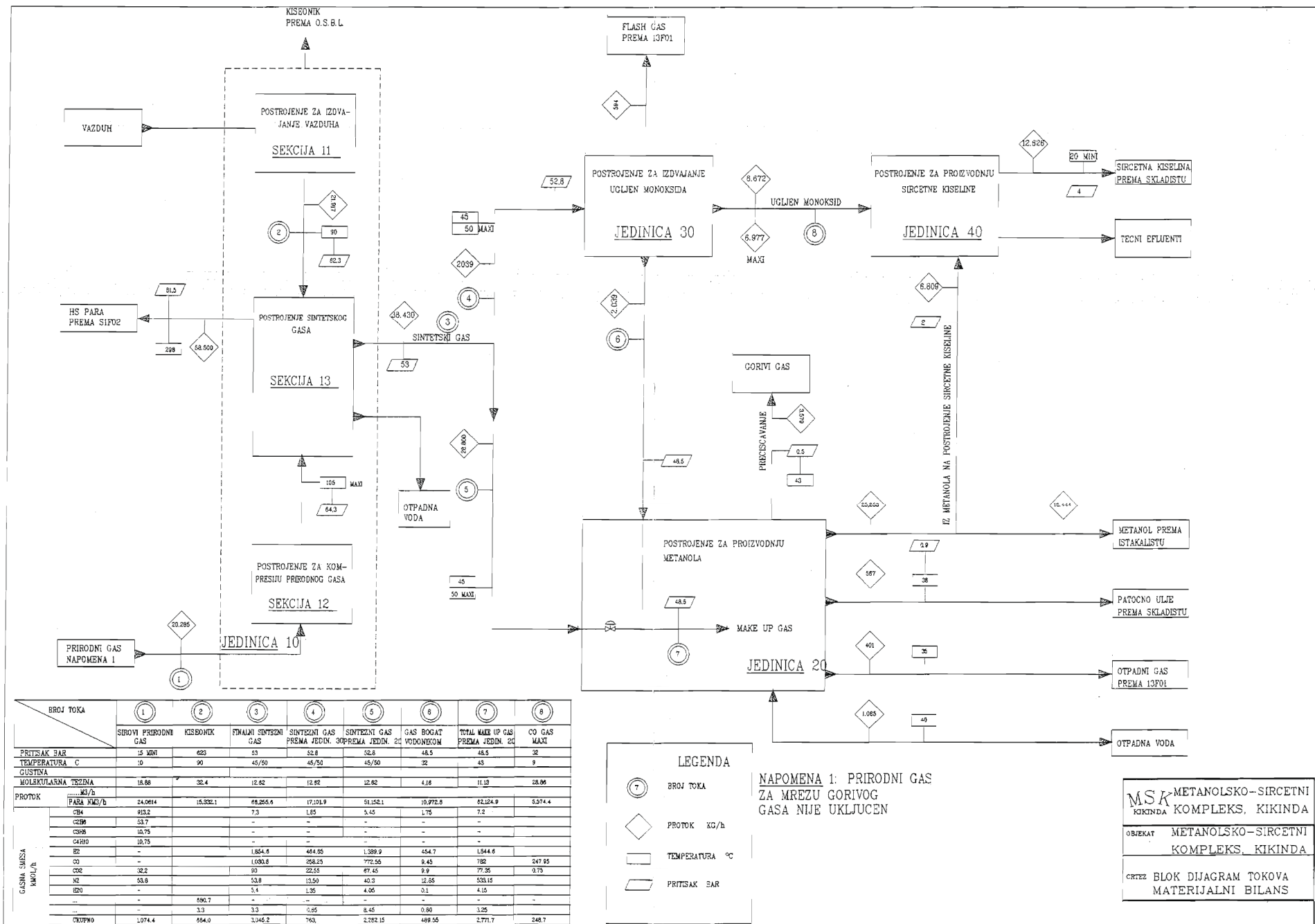
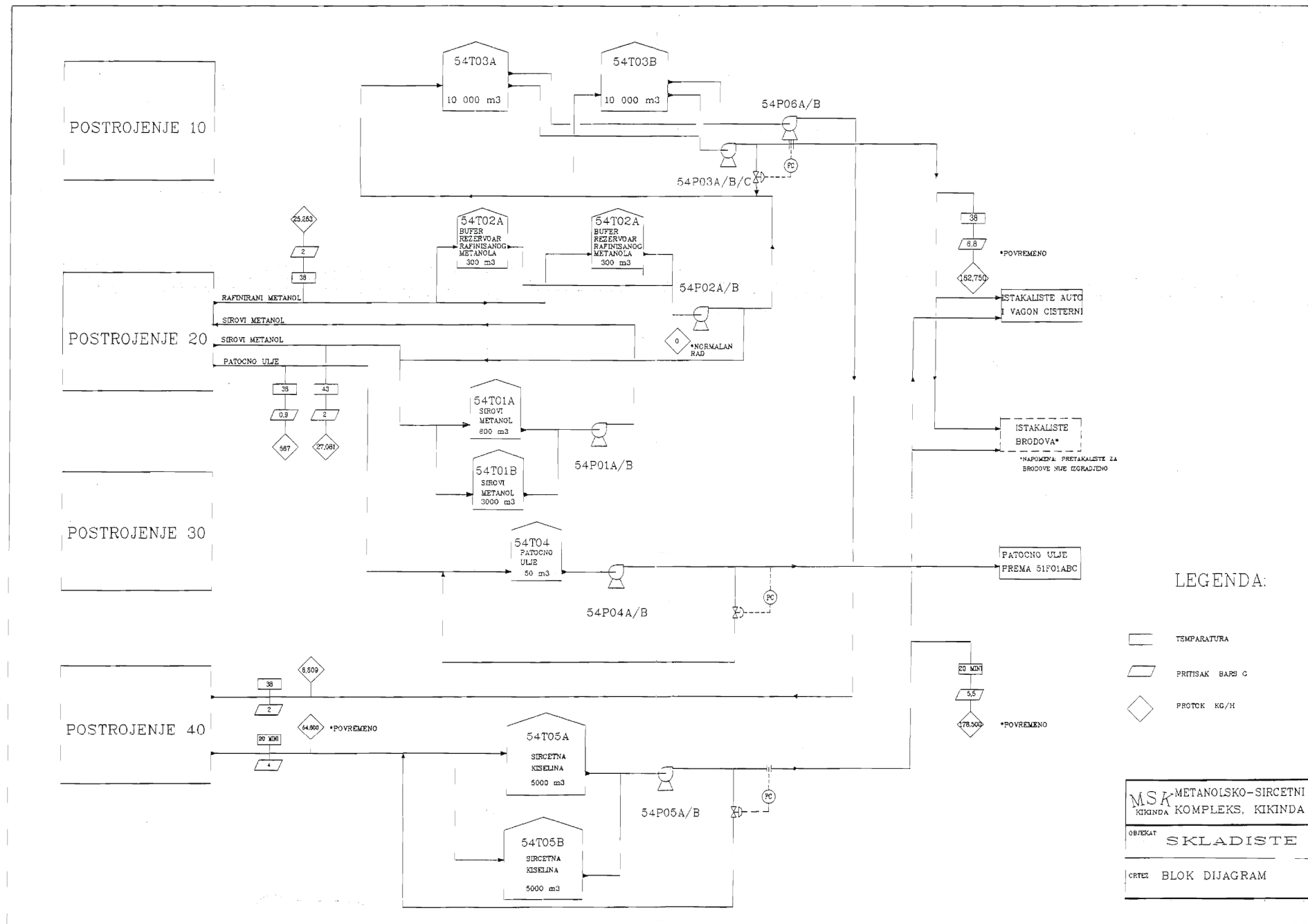
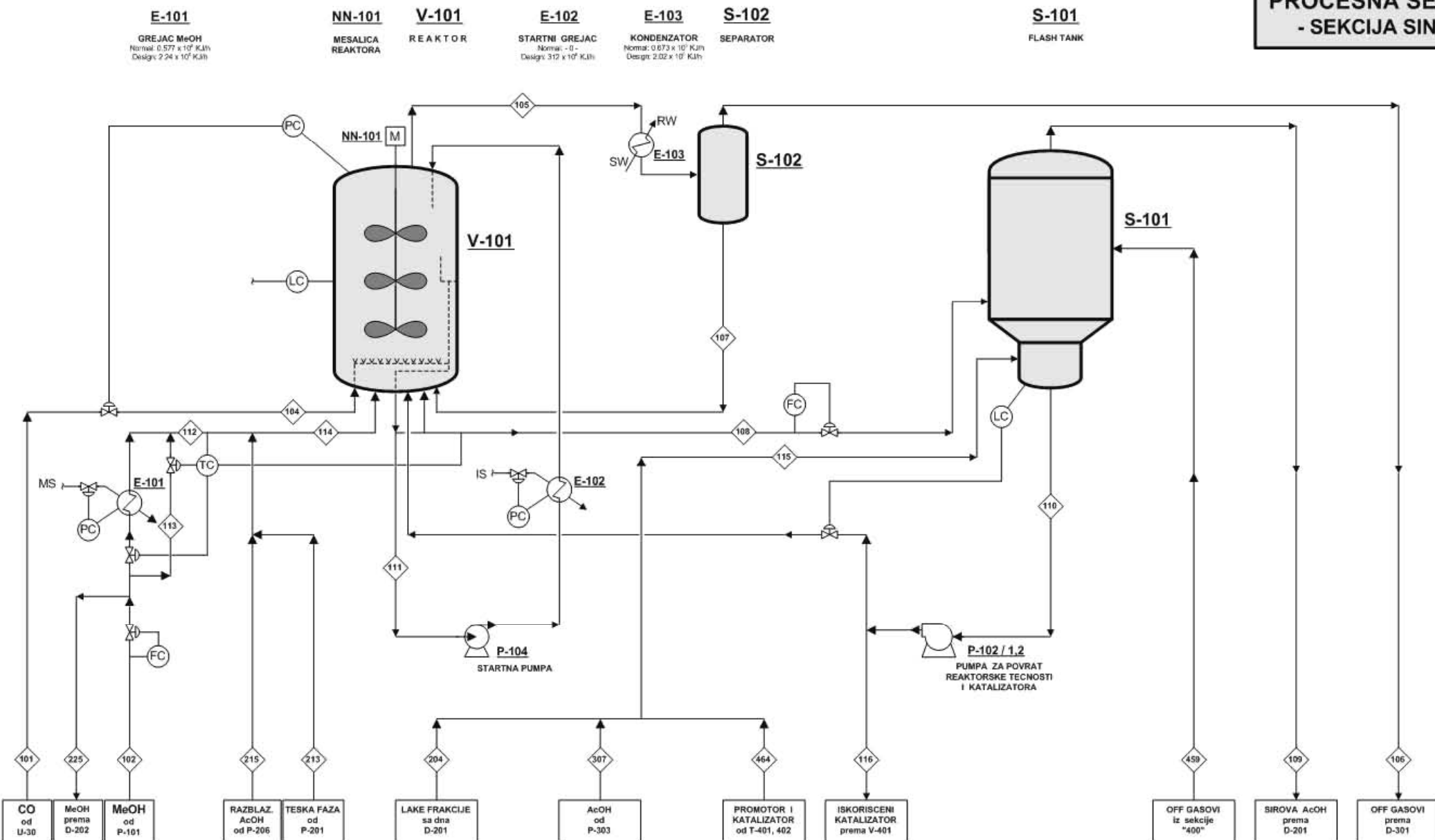




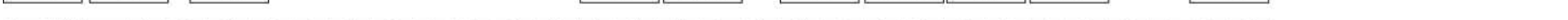


PROCESNA SEMA U-40 - SEKCIJA SINTEZE -



STREAM	1	2	3	4	5	6	7	8	9	10	11	12	13	14	15	16	17	18	19	20	21	22	23	24	25	26	27	28	29	30
KOMPONENTE	1	2	3	4	5	6	7	8	9	10	11	12	13	14	15	16	17	18	19	20	21	22	23	24	25	26	27	28	29	30
H ₂	2.02	-	-	-	1.43	1.42	0.01	0.09	0.99	-	-	-	-	TRACE	-	-	-	-	-	-	TRACE	TRACE	-	-	-	-	-	-	-	-
CH ₄	16.03	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
CO	26.01	1.20	-	-	1.20	0.56	0.55	TRACE	0.65	0.65	TRACE	-	-	0.01	-	-	-	-	-	-	TRACE	TRACE	-	-	-	-	-	-	-	-
CO ₂	26.01	238.54	-	-	238.54	18.94	15.92	0.12	7.64	7.63	0.01	-	-	0.06	-	-	-	-	-	-	0.05	0.01	-	-	-	-	-	-	-	-
CH ₃ COOH	44.01	-	-	-	-	0.33	0.31	0.04	2.34	2.30	0.04	-	-	0.33	-	-	-	-	-	-	0.28	0.05	-	-	-	-	-	-	-	-
CH ₃ COOCH ₃	32.04	-	212.01	-	-	0.02	TRACE	0.02	1.56	0.95	0.58	-	-	210.89	139.19	211.70	TRACE	-	-	-	0.12	0.70	1.12	TRACE	-	-	-	-	-	-
CH ₃ COOCH ₂ CH ₃	141.36	-	-	-	-	4.61	0.73	3.88	101.52	90.32	11.20	-	-	-	-	91.14	TRACE	-	-	-	TRACE	84.78	6.36	-	-	-	-	-	-	-
CH ₃ COOCH ₂ CH ₂ CH ₃	74.08	-	-	-	-	0.34	0.02	0.32	15.14	11.75	4.00	-	-	-	-	12.94	TRACE	-	-	-	0.01	19.43	2.51	-	-	-	-	-	-	-
H ₂ O	66.05	-	-	-	-	4.21	0.01	4.20	1689.39	332.84	1372.98	-	-	-	-	100.48	16.21	-	-	-	14.89	12.52	80.96	-	-	-	-	-	-	-
CH ₃ COOCH ₂ CH ₂ CH ₂ CH ₃	18.02	-	0.38	-	-	5.63	0.05	5.58	1144.76	305.32	848.70	-	-	0.37	0.25	300.16	5.04	-	-	-	0.91	7.47	292.32	TRACE	0.03	-	-	-	-	-
CH ₃ COOCH ₂ CH ₂ CH ₂ CH ₂ CH ₃	127.91	-	-	-	-	0.01	-	0.01	37.35	0.39	37.17	-	-	-	-	-	-	-	-	-	0.28	-	-	-	-	-	-	-	-	-
CH ₃ COOCH ₂ CH ₂ CH ₂ CH ₂ CH ₂ CH ₃	74.08	-	-	-	-	-	-	-	1.85	0.25	1.60	-	-	-	-	-	-	-	-	-	0.03	-	-	-	-	-	-	-	-	-
CH ₃ COOCH ₂ CH ₂ CH ₂ CH ₂ CH ₂ CH ₂ CH ₃	102.91	-	-	-	-	-	-	-	0.47	-	0.47	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
CH ₃ COOCH ₂ CH ₂ CH ₂ CH ₂ CH ₂ CH ₂ CH ₂ CH ₃	85.07	-	0.92	-	-	-	-	-	-	-	-	-	-	0.01	0.01	0.01	-	-	-	-	-	-	TRACE	-	-	-	-	-	-	-
CH ₃ COOCH ₂ CH ₂ CH ₂ CH ₂ CH ₂ CH ₂ CH ₂ CH ₂ CH ₃	238.74	-	-	-	238.74	33.20	10.29	14.8	3004.6	753.06	2216.73	-	-	211.27	139.45	719.83	22.46	-	-	-	21.12	115.85	392.81	1.12	1.34	-	-	-	-	-
UKUPAN PROTOK	kg/h	8715	6800	-	6715	1519	895	934	143016	39626	104567	-	-	8763	5022	32319	1120	-	-	-	1040	13710	11943	36	75	-	-	-	-	-
ZAPREMIN PROTOK	m ³ /h	185.3	8.7	-	199.8	40.9	17.3	0.643	158.0	9289	109.2	-	-	8.5	8.7	28.1	1.2	-	-	-	1.1	7.3	11.4	0.05	0.68	-	-	-	-	-
GUSTINA	kg/m ³	36.24	785	-	33.61	37.14	32.80	1452	900.4	4.27	998	-	-	790.3	785	1152	940.7	-	-	-	934.2	1891	1039	785.1	1029	-	-	-	-	-
MOĆNAJA VASA	kg/m ³	28.01	32.01	-	28.01	45.75	30.79	89.87	27.80	32.50	45.92	-	-	32.01	32.01	44.90	49.34	-	-	-	48.24	118.95	36.14	32.84	99.40	-	-	-	-	-
TEMPERATURA	°C	32	32	-	32	185	49	49	185	128	128	-	-	64	64	128	128	-	-	-	137	49	55	32	38	-	-	-	-	-
PROTISAK (aps.)	bar	32.41	-	-	-	28.59	28.52	28.52	28.59	2.25	2.28	-	-	-	-	-	2.28	-	-	-	2.30	-	-	-	-	-	-	-	-	-

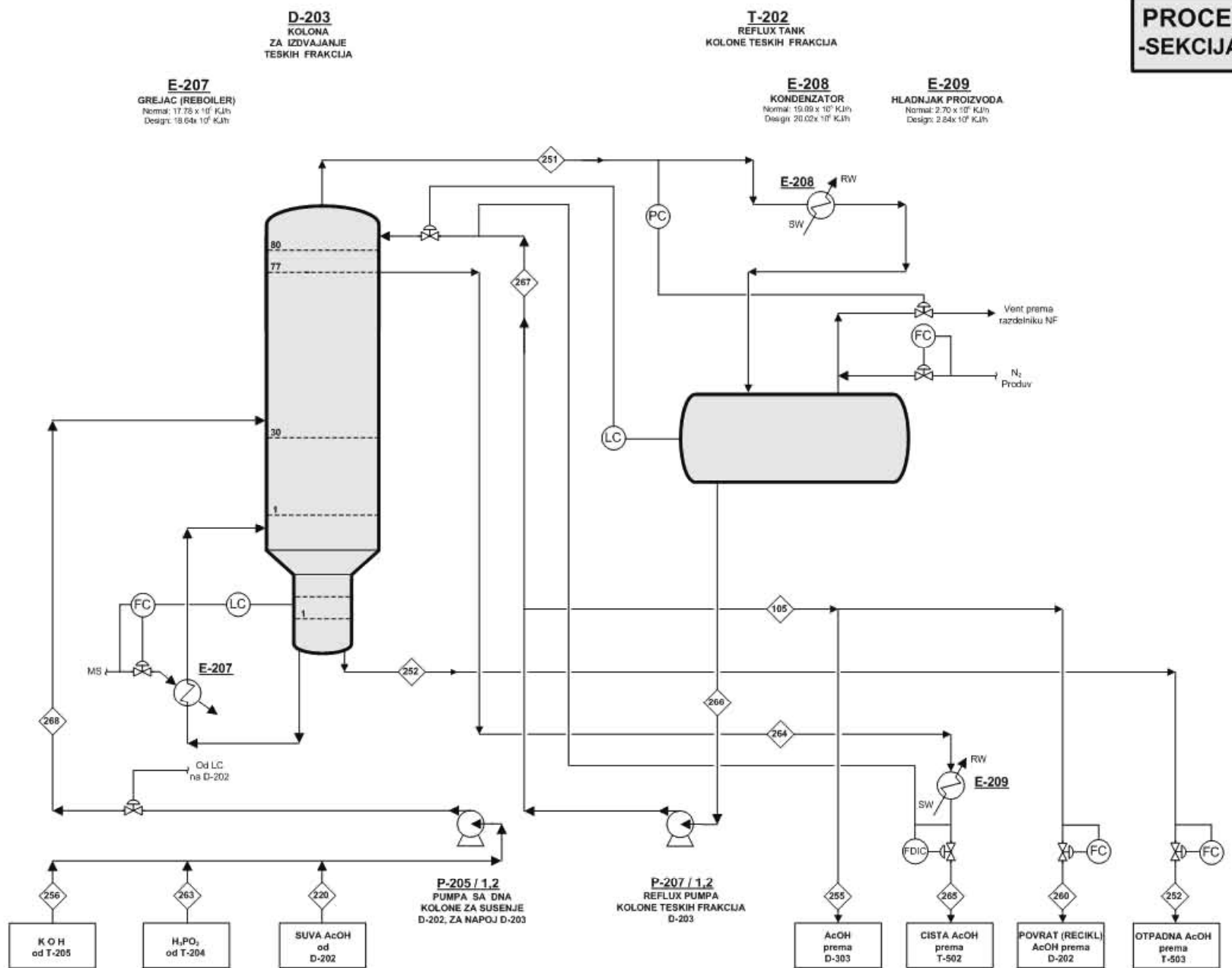
MSK KIKINDA	Naziv:	Procesna Sema - Jedinica Za Proizvodnju Siracetne Kiseline - Sekcija Reakcije - (1)		
	Process Flow Diagram Acetic Acid Plant Reaction			
Projektant:	Projekantska oznaka:	MSK sifra:		
Monsanto Company	41190-1	MSK-PS-2120-01		
Izdavanje br: 01	Datum:	15.06.1998.	Primerak br:	00
Autor izmene:	Overtio:	Odobrio:		
Malencic Uros	Milovanov Branislava	Miskovic Dusan		



STREAM 10"		MW																		NORMAL 10"																	
KOMPONENTE	CHL	1	2	3	4	5	6	7	8	9	10	11	12	13	14	15	16	17	18	19	20	21	22	23	24	25	26	27	28								
H ₂	2.02	0.30	TRACE	TRACE	-	-	0.31	TRACE	TRACE	-	-	TRACE	-	-	TRACE	TRACE	TRACE	0.91	-	-	TRACE	TRACE	-	TRACE	0.90	-	-	0.91	-								
CH ₄	26.01	0.65	TRACE	TRACE	-	-	0.68	TRACE	TRACE	0.66	-	0.66	0.60	TRACE	TRACE	-	TRACE	-	-	-	-	-	-	-	0.65	-	-	-	0.91								
CO	26.01	7.83	0.91	0.91	-	-	7.85	0.05	0.02	7.91	TRACE	7.85	7.24	0.01	0.05	TRACE	0.91	-	-	-	-	-	-	TRACE	0.93	-	-	-	0.96								
CO ₂	44.01	2.60	0.04	0.06	TRACE	-	3.00	0.28	0.10	3.00	0.01	3.00	2.82	0.08	0.28	0.01	0.05	-	-	-	-	-	TRACE	0.01	0.03	-	0.03	0.02	0.45								
CH ₃ OH	32.06	0.98	0.70	1.11	0.02	TRACE	0.63	0.12	1.81	1.94	0.19	0.03	0.01	0.02	0.12	-	0.70	-	-	-	-	-	TRACE	0.01	0.03	-	0.03	0.02	0.45								
C ₂ H ₅ OH	30.24	5.24	3.78	5.24	0.37	TRACE	36.38	0.42	3.49	36.38	0.42	2.45	2.45	0.24	24.76	22.46	24.76	-	-	-	-	-	TRACE	0.01	0.03	-	0.03	0.02	0.45								
C ₃ H ₇ COOH	74.08	11.75	1.33	2.15	-	0.51	0.82	10.43	3.80	13.90	-	-	0.32	0.07	0.75	10.43	1.13	2.51	-	-	-	-	TRACE	0.01	0.03	-	0.03	0.02	0.45								
C ₃ H ₇ CH ₂ OH	60.05	332.64	45.25	72.64	35.82	14.09	0.16	12.52	117.89	130.41	287.47	0.16	TRACE	0.16	12.52	45.27	30.96	-	-	-	-	-	TRACE	0.01	0.03	-	0.03	0.02	0.45								
H ₂ O	18.02	305.32	149.96	240.78	18.45	0.91	1.26	7.47	390.75	398.32	161.50	1.26	0.10	1.16	7.47	142.36	292.32	-	-	-	-	-	TRACE	0.01	0.03	-	0.03	0.02	0.45								
H ₂	12.01	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	TRACE	0.01	0.03	-	0.03	0.02	0.45								
C ₂ H ₆	74.08	0.28	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	TRACE	0.01	0.03	-	0.03	0.02	0.45								
R _h	102.91	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	TRACE	0.01	0.03	-	0.03	0.02	0.45								
T O T A L		kg/m ³ / h	200.87	322.49	95.70	21.12	29.48	115.65	520.37	653.88	414.61	28.48	14.96	14.62	115.65	192.85	392.91	-	-	-	-	-	TRACE	0.01	0.03	-	0.03	0.02	0.45								
UKUPAN PROTOK		kg/m ³ / h	793.66	1048	971.4	258	296	2565	13710	15763	22428	2565	223	1842	13710	2393	11843	-	-	-	-	-	TRACE	0.01	0.03	-	0.03	0.02	0.45								
ZAPREMIN PROTOK		m ³ / h	9285	5.8	9.3	-	-	372	7.3	15.1	8005	22.5	372	174.4	0.84	7.3	5.6	11.4	-	-	-	-	TRACE	0.01	0.03	-	0.03	0.02	0.45								
GUSTINA		kg / m ³	4027	1047	1047	944.4	81.4	6.69	1890	1048	3.35	944.4	4.89	2185	4.89	1891	1031	1039	-	-	-	-	TRACE	0.01	0.03	-	0.03	0.02	0.45								
MOJ ARIKNA WAKTU		kg / m ³ / h	34.58	30.12	30.12	45.92	42.34	87.02	118.35	30.12	46.17	45.93	87.02	48.36	126.96	118.35	50.16	30.14	-	-	-	-	TRACE	0.01	0.03	-	0.03	0.02	0.45								
TEMPERATURA		°C	120	-	-	-	-	120	-	-	-	-	-	-	-	-	-	-	-	-	-	-	TRACE	0.01	0.03	-	0.03	0.02	0.45								
PROTOK (aps)		bar	2.28	-	-	-	-	2.30	-	2.27	2.07	2.07	2.07	2.04	2.04	2.04	2.04	2.04	-	-	-	-	TRACE	0.01	0.03	-	0.03	0.02	0.45								

	Naziv: Procesna Sema - Jednina Za Proizvodnju Sirovine Kiseline - Soljika Destilacije - (2A)		
	Process Flow Diagram Acetic Acid Plant Purification		
Projektant: Monsanto Company	Projektantska oznaka: 41190-2A	MSK otkr: MSK-PS-2120-02	
Izdati na: 01	Datum: 15.06.1998.	Primerak od: 00	
Autor izmjeni: Malencic Uros	Overio: Milovanov Branislava	Odobrio: Miskovic Dusan	

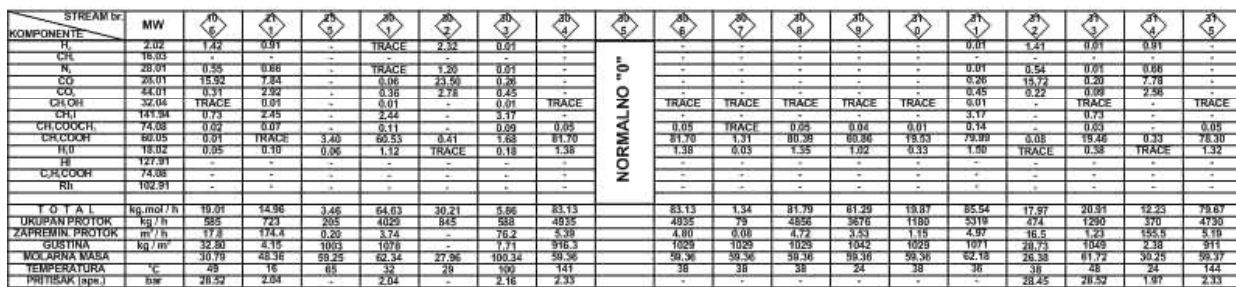
PROCESNA SEMA U-40
-SEKCIJA DESTILACIJE (II)-



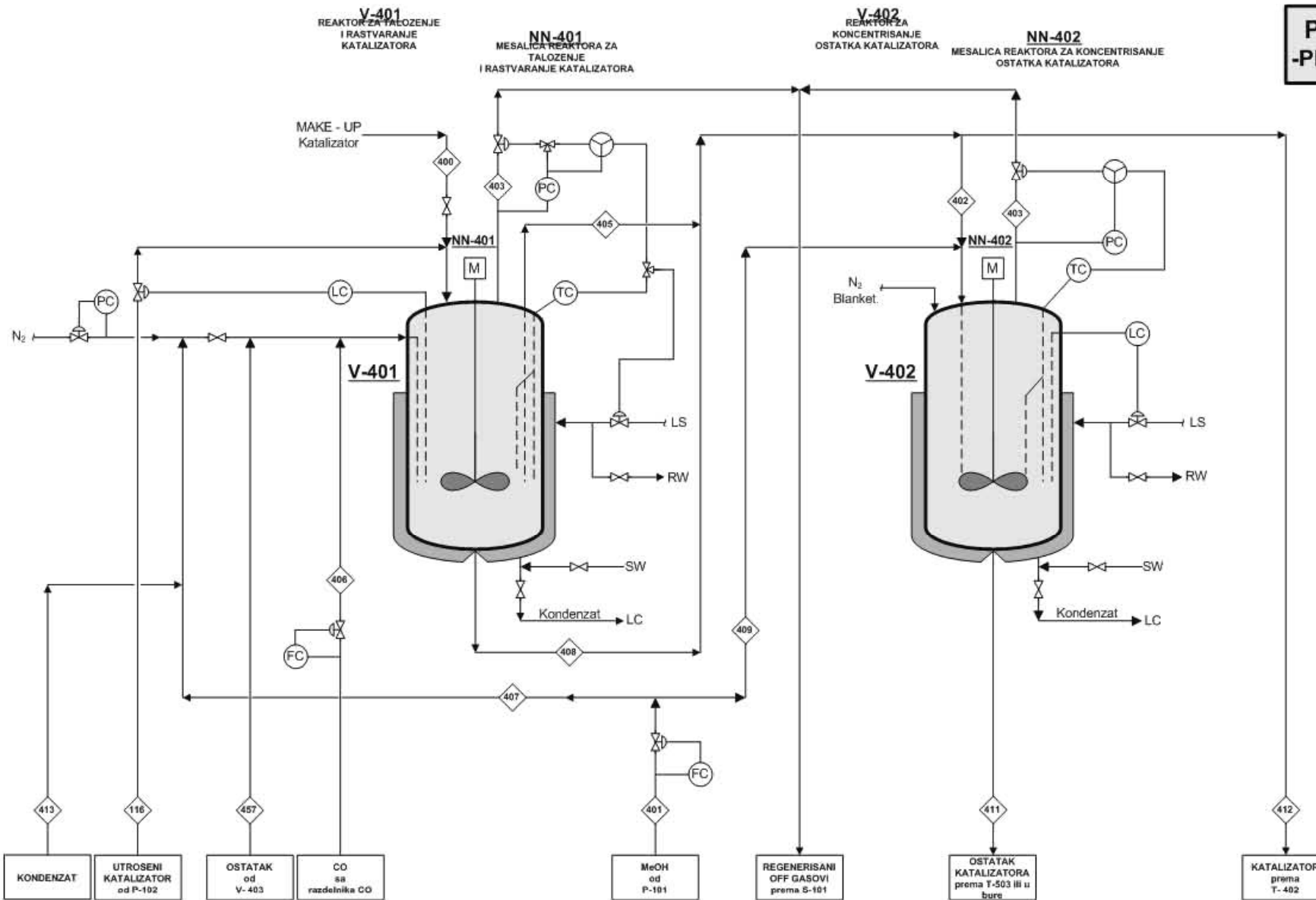
STREAM br.	MW	25	26	27	28	29	30	31	32	33	34	35	36	37	38	39	40
KOMPONENTE																	
H ₂	2.02	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
CH ₄	16.04	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
N ₂	28.01	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
CO	28.01	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
CO ₂	44.01	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
CH ₃ OH	32.04	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
CH ₃ COOH	74.08	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
CH ₃ COOH	60.05	222.35	567.48	1.44	11.0	3.40	-	7.80	-	-	-	-	-	-	-	-	-
H ₂ O	18.02	1.10	0.44	-	0.18	0.06	0.13	0.13	-	-	-	-	-	-	-	-	-
H ₂	127.91	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
CH ₃ COOH	74.08	0.25	0.02	0.24	TRACE	-	-	TRACE	-	-	-	-	-	-	-	-	-
H ₂	102.91	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
KOH	56.10	-	-	-	0.01	-	-	0.01	-	-	-	-	-	-	-	-	-
TOTAL	kg/mol/h	223.70	576.94	1.89	11.18	3.46	0.14	7.73	-	-	-	-	-	-	-	-	-
URUPAN PROTOK	kg/h	13391	24251	195	864	205	3.0	484	-	-	-	-	-	-	-	-	-
ZAPREMIN PROTOK	m ³ /h	15	8857	0.12	0.66	0.20	-	0.46	-	-	-	-	-	-	-	-	-
GUSTINA	kg/m ³	890	3.82	900.3	1003	1003	1238	1003	-	-	-	-	-	-	-	-	-
MOCARNA MASA	kg/h	39.36	59.37	62.91	39.37	59.37	21.43	39.37	-	-	-	-	-	-	-	-	-
TEMPERATURA	°C	161	127	144	65	65	35	65	-	-	-	-	-	-	-	-	-
PRITISAK (aps.)	bar	3.31	1.36	2.10	-	-	-	-	-	-	-	-	-	-	-	-	-

MSK KIKINDA	Naзив: Procesna Sema - Jedinica Za Proizvodnju Sintetne Kiseline - Sekcija Destilacije - (ZB)	MSK ulica
Projekant: Monsanto Company	Projekantska oznaka: 41190-ZB	MSK ulica
izdanje br: 01	Datum: 15.06.1998.	Primerak br: 00
Author izmislja: Malencic Uros	Oviseo: Milovanov Branislava	Odobrio: Miskovic Dusan

	Naziv: Procesna Sema - Jedinica Za Proizvodnju Siroetine Kiseline - Sekcija Za Izdvojavanje Lakih Frakcija - (3) Process Flow Diagram Acetic Acid Plant Light Ends Recovery		
	Projektant: Monsanto Company	Projektantsko oznaka: 41190-3	MSK štifa: MSK-PS-2120-04
Izdavanje br: 01	Datum: 15.06.1998.	Primak br: 00	
Autor izmjene: Malenčic Uros	Ovećen: Milovanov Branislava	Odobrio: Miskovic Dusan	

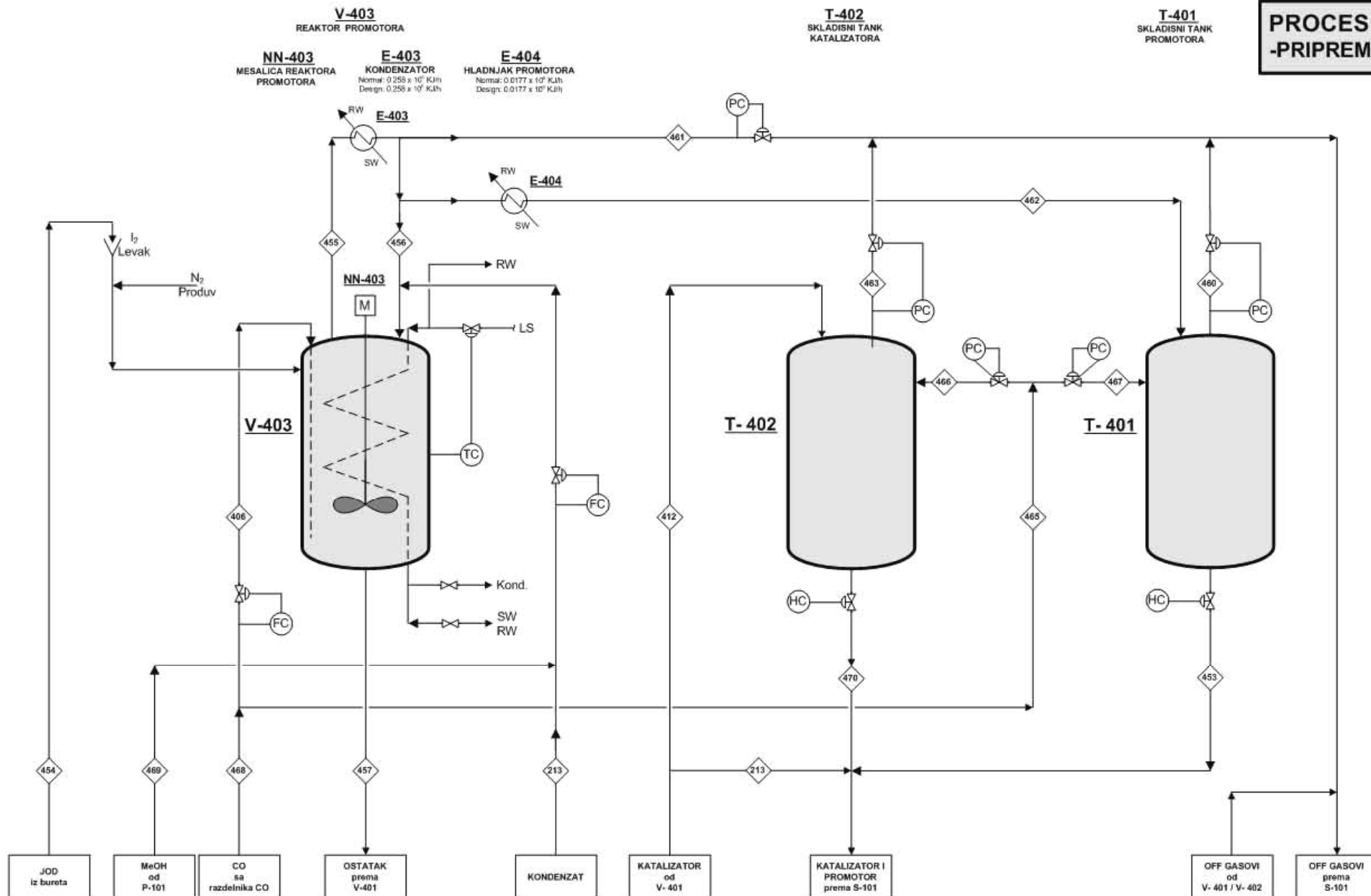


PROCESNA SEMA U-40 -PRIPREMA KATALIZATORA-



OPERACIJA		REAKTOR, V-401, TALOZENJE										REAKTOR, V-401, RASTVARANJE										REAKTOR, V-402, KONC.				R A Z N O		
STREAM br.	MW	6 A	1 V	2 V	V-401 Kont.	3 A	V-401 Kont.	5 V	V-401 Kont.	7 B	8 V	V-401 Kont.	6 V	3 B	8 V	2 V	V-402 Kont.	9 V	1 V	7 V	9 V	3 V						
KOMPONENTE																												
N ₂	2.02	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-						
H ₂ O	28.01	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-						
CO	28.01	0.01	-	-	0.01	0.01	-	-	-	-	-	-	0.01	-	-	-	-	-	-	-	-	-						
CO ₂	44.01	0.04	-	-	0.04	0.04	-	-	-	-	-	-	0.03	-	-	-	-	-	-	-	-	-						
CH ₃ COOH	32.04	0.47	-	-	0.50	0.50	-	-	-	-	-	-	0.41	-	-	-	-	-	-	-	-	-						
CH ₃ COOCH ₃	74.08	38.05	-	-	148.30	153.72	8.55	8.71	0.84	34.37	-	-	35.21	-	-	-	-	-	-	-	-	-						
CH ₃ COOCH ₂ CH ₃	60.05	7.43	-	-	288.13	196.09	92.04	83.09	8.05	8.21	-	-	54.48	-	-	1.06	11.33	83.99	83.38	8.11	-	-						
H ₂ O	18.02	383.30	0.15	-	467.47	83.18	384.29	350.68	33.01	330.69	-	-	1933.77	-	-	82.25	1891.52	1576.24	1396.10	180.14	-	-						
H ₂	1.01	127.91	119.21	-	7.08	7.08	7.28	0.70	102.03	101.53	-	-	368.27	-	-	19.03	368.27	320.88	334.14	16.54	-	-						
CH ₃ COOH	74.08	2.98	-	-	2.98	-	2.98	2.72	0.26	2.57	-	-	103.53	-	-	2.83	103.53	7.28	7.28	-	-	-						
RH	102.91	1.21	-	-	1.21	-	1.21	0.02	1.19	1.04	-	-	2.83	-	-	2.83	2.72	2.72	2.72	-	-	-						
METALI	13.71	-	-	-	13.17	-	13.17	12.02	1.15	11.36	-	-	12.51	-	-	12.51	12.02	12.02	12.02	-	-	-						
TOTAL	2634.30	139.45	2783.85	545.42	2238.53	2041.66	196.78	2272.42	2448.20	93.47	221.58	2341.18	2041.66	1822.61	218.85	-	-	-	-	-	-	-						
TEMPERATURA	°C	128	32	121	50	150	150/40	49	128	122	32	120	120/49	49	135	135/49	-	-	-	-	-	-						
PRITISAK (abs.)	bar	-	-	-	5.5/2.4	2.4	-	2.4	-	6.9	6.9	-	7.4	5.5/2.4	-	-	-	-	-	-	-	-						
GUSTINA	kg/m ³	936	784.8	970	81	916	1026	976	958	959	7.1	8.5	1040	1020	9.8	1010	-	-	-	-	-	-						

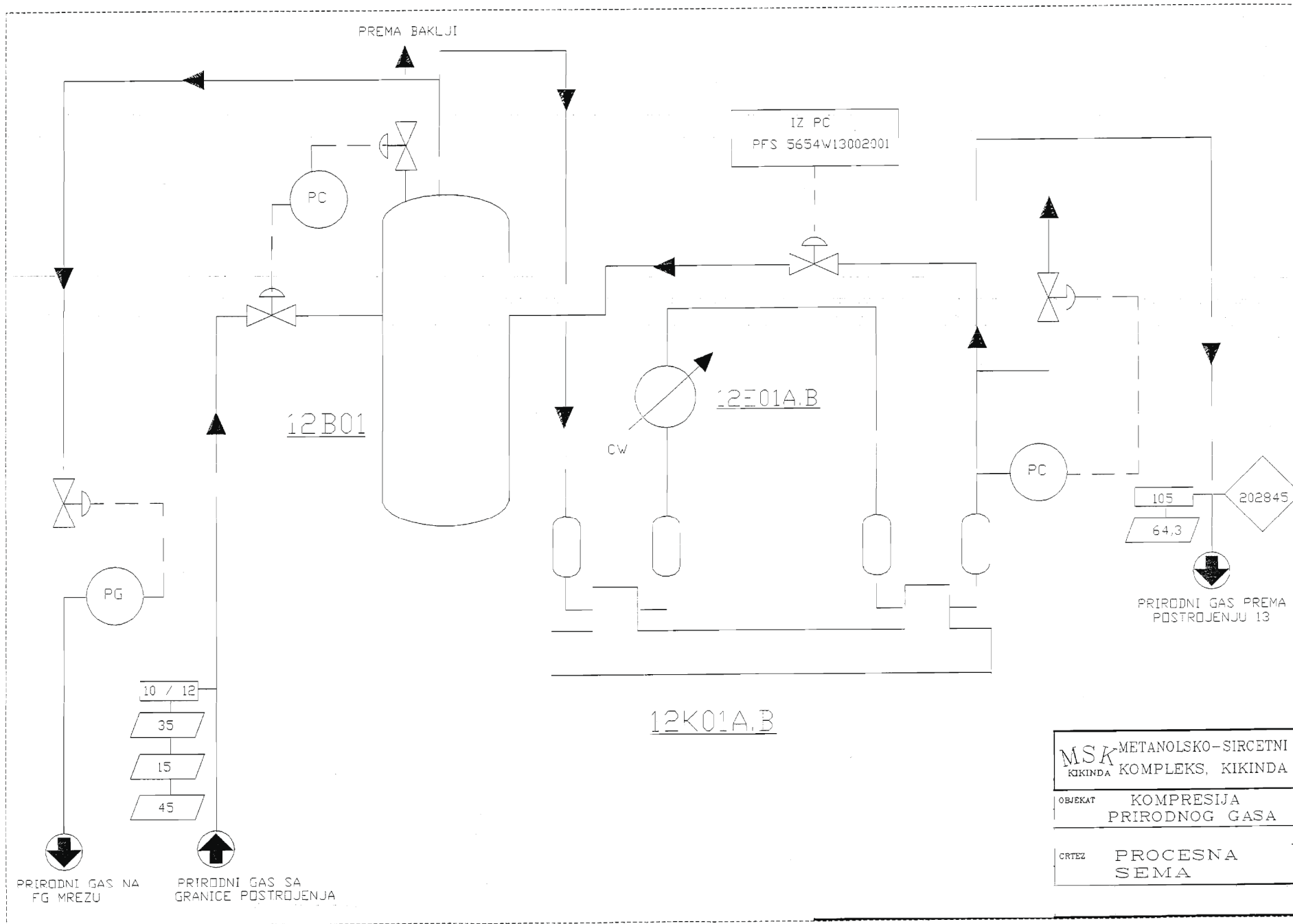
MSK KIKINDA		Naziv: Procesna Sema - Jedinica Za Proizvodnju Sirćetne Kiseline - Priprema Katalizatora - (4A)	
Projektant: Monsanto Company		Projekantska oznaka: 41190-4A	
Izdavanje br: 01		Datum: 15.06.1998.	
Autor: Malencic Uros		Odobrio: Milovanov Branislava	
		Primerak br: 00	
		MSK skica: MSK-PS-2120-05	
		Odobrio: Miskovic Dusan	

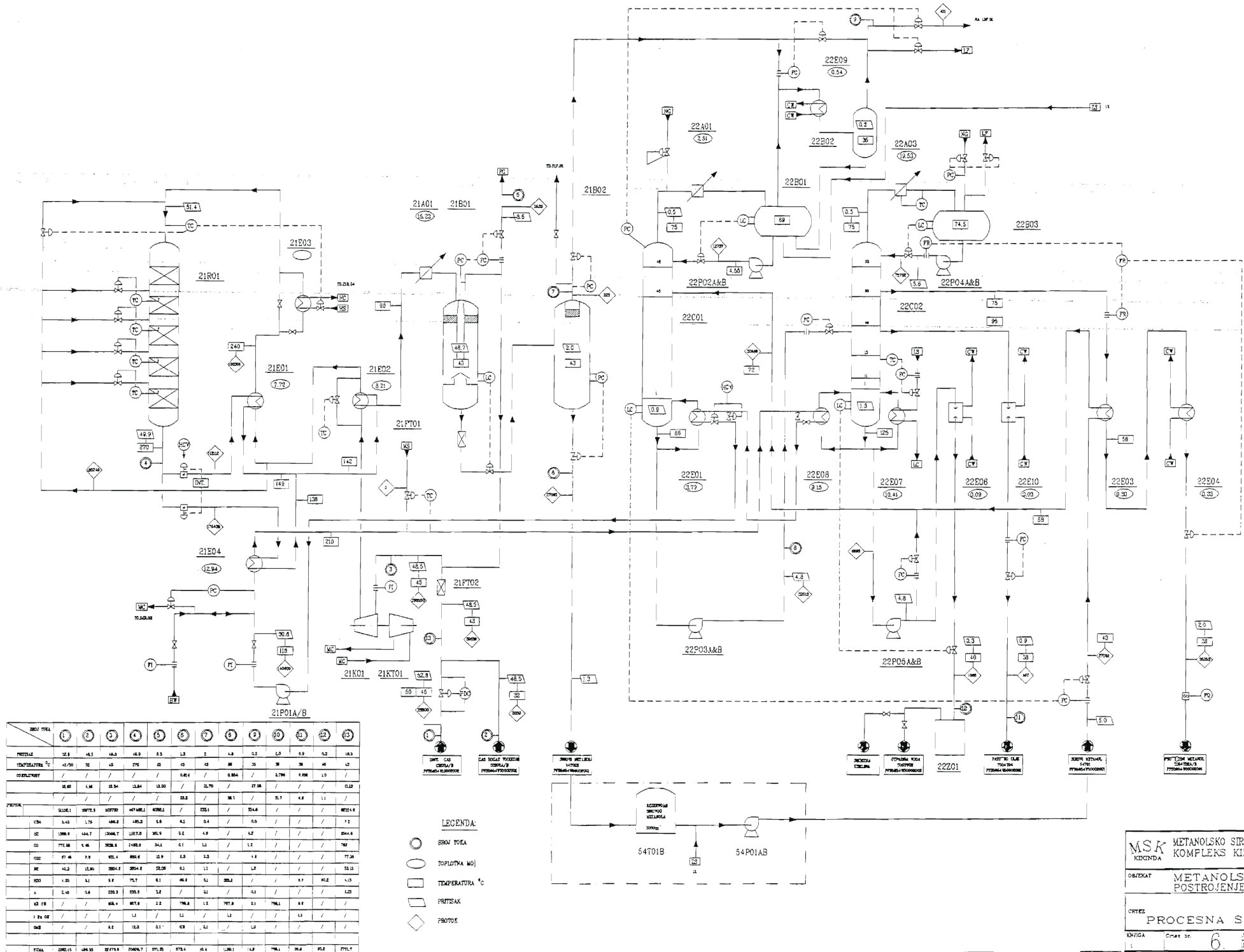


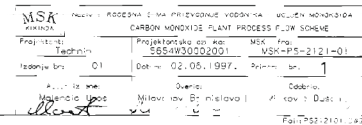
OPERACIJA		REAKTOR, V-403, PROIZVODNJA VODONIK-JODIDA										REAKTOR, V-403, PROIZVODNJA METIL-JODIDA										SKLADISTENJE KATALIZATORA I PROMOTORA									
STREAM br.	MW	V-403 Kont.	1	2	3	4	5	6	V-403 Kont.	Ohladjeno, bez pritiska	7	V-403 Kont.	8	V-403 Kont.	9	10	11	12	13	14	15	16	17	18	19	20	21	22	23	24	25
KOMPONENTE																															
H ₂	2.02	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
N ₂	28.01	-	-	-	2.39	2.39	2.39	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
CO	28.01	-	-	-	476.27	360.16	360.16	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
CO ₂	44.01	-	-	-	141.55	141.55	141.55	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
CH ₃ OH	32.04	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
CH ₃	141.34	4.54	-	4.54	-	4.54	4.54	TRACE	-	207.06	0.31	0.31	0.31	4.54	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
CH ₃ COOH	74.08	-	-	-	-	-	-	-	-	-	913.24	808.70	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
CH ₃ COO	60.05	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
H ₂ O	18.02	2351.42	-	2351.42	-	10.43	221.35	210.92	2283.02	2283.02	-	2308.90	47.48	2351.42	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
HI	127.91	1257.36	-	1257.36	-	TRACE	12.25	12.25	2000.33	2000.33	-	-	-	1257.36	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
C ₂ H ₅ COOH	74.08	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
HS	102.51	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
ME	253.80	-	816.47	816.47	-	TRACE	0.80	0.80	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
TOTAL	kg / sek	3613.32	816.47	4429.79	478.66	545.10	778.25	233.15	4363.35	4363.35	207.06	4570.41	897.09	3613.32	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
	°C	32	27	32	32	32	32	32	32	32	32	32	32	32	32	32	32	32	32	32	32	32	32	32	32	32	32	32	32	32	32
TEMPERATURA	°C	32	27	32	32	32	32	32	32	32	32	32	32	32	32	32	32	32	32	32	32	32	32	32	32	32	32	32	32	32	32
PRITISAK (abs.)	kg / m ²	1330	2400	1530	7.4	6.6-2.4	6.6-2.4	6.6-2.4	6.6-2.4	6.6-2.4	1230	1460	785	1380	2140	1270	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
	kg / m ³	1330	2400	1530	7.4	6.6-2.4	6.6-2.4	6.6-2.4	6.6-2.4	6.6-2.4	1230	1460	785	1380	2140	1270	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
	kg / m ³	1330	2400	1530	7.4	6.6-2.4	6.6-2.4	6.6-2.4	6.6-2.4	6.6-2.4	1230	1460	785	1380	2140	1270	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
	kg / m ³	1330	2400	1530	7.4	6.6-2.4	6.6-2.4	6.6-2.4	6.6-2.4	6.6-2.4	1230	1460	785	1380	2140	1270	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
	kg / m ³	1330	2400	1530	7.4	6.6-2.4	6.6-2.4	6.6-2.4	6.6-2.4	6.6-2.4	1230	1460	785	1380	2140	1270	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
	kg / m ³	1330	2400	1530	7.4	6.6-2.4	6.6-2.4	6.6-2.4	6.6-2.4	6.6-2.4	1230	1460	785	1380	2140	1270	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
	kg / m ³	1330	2400	1530	7.4	6.6-2.4	6.6-2.4	6.6-2.4	6.6-2.4	6.6-2.4	1230	1460	785	1380	2140	1270	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
	kg / m ³	1330	2400	1530	7.4	6.6-2.4	6.6-2.4	6.6-2.4	6.6-2.4	6.6-2.4	1230	1460	785	1380	2140	1270	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
	kg / m ³	1330	2400	1530	7.4	6.6-2.4	6.6-2.4	6.6-2.4	6.6-2.4	6.6-2.4	1230	1460	785	1380	2140	1270	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
	kg / m ³	1330	2400	1530	7.4	6.6-2.4	6.6-2.4	6.6-2.4	6.6-2.4	6.6-2.4	1230	1460	785	1380	2140	1270	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
	kg / m ³	1330	2400	1530	7.4	6.6-2.4	6.6-2.4	6.6-2.4	6.6-2.4	6.6-2.4	1230	1460	785	1380	2140	1270	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
	kg / m ³	1330	2400	1530	7.4	6.6-2.4	6.6-2.4	6.6-2.4	6.6-2.4	6.6-2.4	1230	1460	785	1380	2140	1270	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
	kg / m ³	1330	2400	1530	7.4	6.6-2.4	6.6-2.4	6.6-2.4	6.6-2.4	6.6-2.4	1230	1460	785	1380	2140	1270	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
	kg / m ³	1330	2400	1530	7.4	6.6-2.4	6.6-2.4	6.6-2.4	6.6-2.4	6.6-2.4	1230	1460	785	1380	2140	1270	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
	kg / m ³	1330	2400	1530	7.4	6.6-2.4	6.6-2.4	6.6-2.4	6.6-2.4	6.6-2.4	1230	1460	785	1380	2140	1270	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
	kg / m ³	1330	2400	1530	7.4	6.6-2.4	6.6-2.4	6.6-2.4	6.6-2.4	6.6-2.4	1230	1460	785	1380	2140	1270	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
	kg / m ³	1330	2400	1530	7.4	6.6-2.4	6.6-2.4	6.6-2.4	6.6-2.4	6.6-2.4	1230	1460	785	1380	2140	1270	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
	kg / m ³	1330	2400	1530	7.4	6.6-2.4	6.6-2.4	6.6-2.4	6.6-2.4	6.6-2.4	1230	1460	785	1380	2140	1270	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
	kg / m ³	1330	2400	1530	7.4	6.6-2.4	6.6-2.4	6.6-2.4	6.6-2.4	6.6-2.4	1230	1460	785	1380	2140	1270	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
	kg / m ³	1330	2400	1530	7.4	6.6-2.4	6.6-2.4	6.6-2.4	6.6-2.4	6.6-2.4	1230	1460	785	1380	2140	1270	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
	kg / m ³	1330	2400	1530	7.4	6.6-2.4	6.6-2.4	6.6-2.4	6.6-2.4	6.6-2.4	1230	1460	785	1380	2140	1270	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
	kg / m ³	1330	2400	1530	7.4	6.6-2.4	6.6-2.4	6.6-2.4	6.6-2.4	6.6-2.4	1230	1460	785	1380	2140	1270	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
	kg / m ³	1330	2400	1530	7.4	6.6-2.4	6.6-2.4	6.6-2.4	6.6-2.4	6.6-2.4	1230	1460	785	1380	2140	1270	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
	kg / m ³	1330	2400	1530	7.4	6.6-2.4	6.6-2.4	6.6-2.4	6.6-2.4	6.6-2.4	1230	1460	785	1380	2140	1270	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
	kg / m ³	1330	2400	1530	7.4	6.6-2.4	6.6-2.4	6.6-2.4	6.6-2.4	6.6-2.4	1230	1460	785	1380	2140	1270	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
	kg / m ³	1330	2400	1530	7.4	6.6-2.4	6.6-2.4	6.6-2.4	6.6-2.4	6.6-2.4	1230	1460	785	1380	2140	1270	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
	kg / m ³	1330	2400	1530	7.4	6.6-2.4	6.6-2.4	6.6-2.4	6.6-2.4	6.6-2.4	1230	1460	785	1380	2140	1270	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
	kg / m ³	1330	2400	1530	7.4	6.6-2.4	6.6-2.4	6.6-2.4	6.6-2.4	6.6-2.4	1230	1460	785	1380	2140	1270	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
	kg / m ³	1330	2400	1530	7.4	6.6-2.4	6.6-2.4	6.6-2.4	6.6-2.4	6.6-2.4	1230	1460	785	1380	2140	1270	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
	kg / m ³	1330	2400	1530	7.4	6.6-2.4	6.6-2.4	6.6-2.4	6.6-2.4	6.6-2.4	1230	1460	785	1380	2140	1270	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
	kg / m ³	1330	2400	1530	7.4	6.6-2.4	6.6-2.4	6.6-2.4	6.6-2.4	6.6-2.4	1230	1460	785	1380	2140	1270	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
	kg / m ³	1330	2400	1530	7.4	6.6-2.4	6.6-2.4	6.6-2.4	6.6-2.4	6.6-2.4	1230	1460	785	1380	2140	1270	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
	kg / m ³	1330	2400	1530	7.4	6.6-2.4	6.6-2.4	6.6-2.4	6.6-2.4	6.6-2.4	1230	1460	785	1380	2140	1270	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
	kg / m ³	1330	2400	1530	7.4	6.6-2.4	6.6-2.4	6.6-2.4	6.6-2.4	6.6-2.4	1230	1460	785	1380	2140	1270	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
	kg / m ³	1330	2400	1530	7.4	6.6-2.4	6.6-2.4	6.6-2.4	6.6-2.4	6.6-2.4	1230	1460	785	1380	2140	1270	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
	kg / m ³	1330	2400	1530	7.4	6.6-2.4	6.6-2.4	6.6-2.4	6.6-2.4	6.6-2.																					

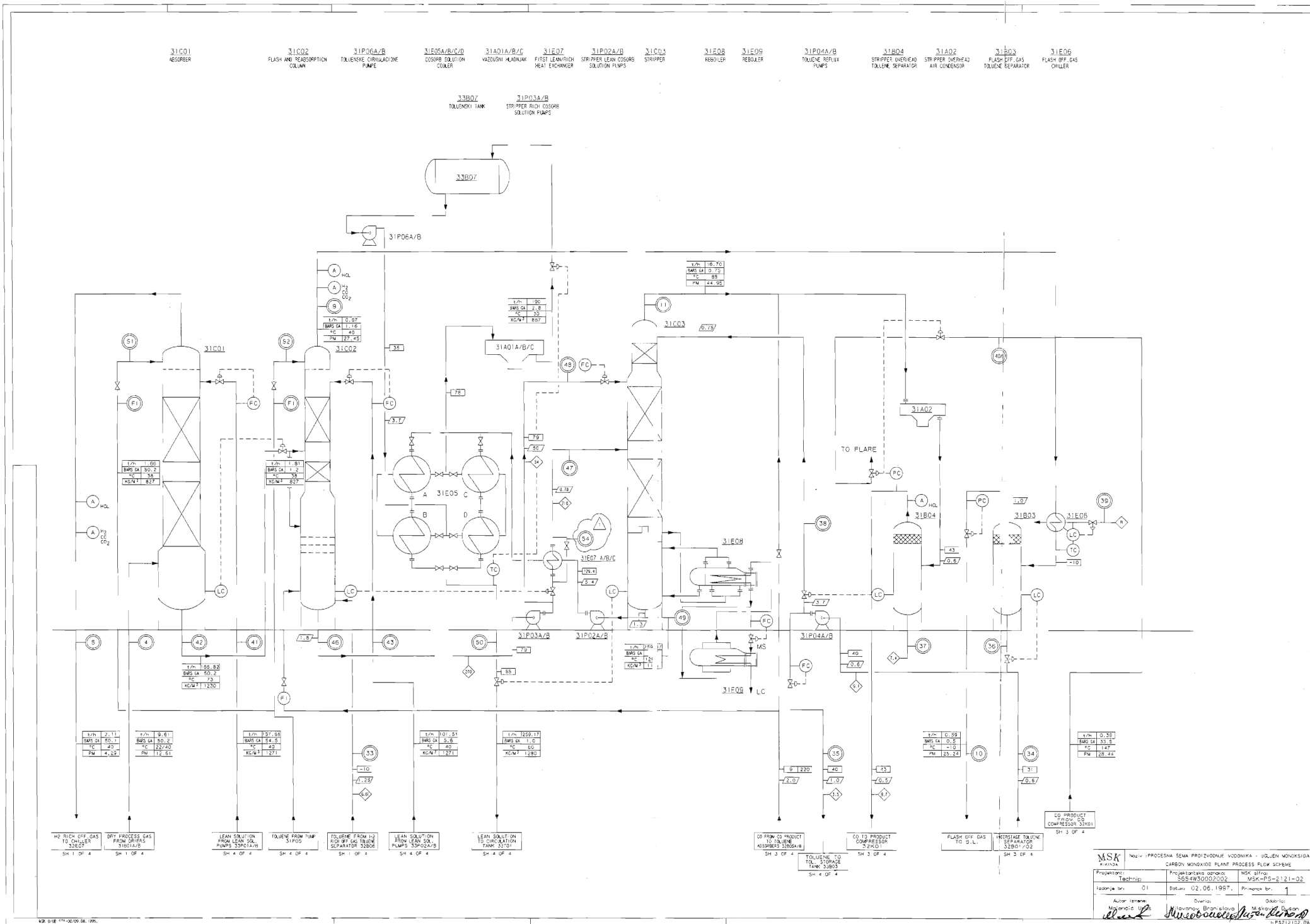
PROCESNA SEMA U-40 -PRIPREMA PROMOTORA-

MSK KIKINDA		Naziv: Procesna Sema - Jedinica Za Proizvodnju Sirćetne Kiseline - Priprema Promotora - (4B)	
Projektant: Monsanto Company		Projektantska oznaka: 41190-4B	
Indeks br. 01		Datum: 15.06.1998.	
Autor: Malencic Uros		Odobrio: Milovanovic Brankislava	
		MSK skica: MSK-PS-2120-06	
		Prilozak br. 00	
		Odobrio: Miskovic Dusan	

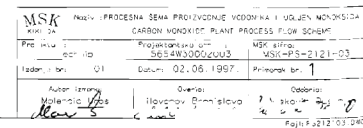








32E05
CO PRODUCT
REGENERATION
GAS HEATER



33P01A/B
ABSORBER LEAN COSORB
SOLUTION PUMPS

33P02A/B
ABSORBER LEAN COSORB
SOLUTION PUMPS

33T01A/B
COSORB
CIRCULATION TANK

33T02
TOLUENE WASH
TANK

33B03
TOLUENE
STORAGE TANK

33P03A/B
FLUSHING PUMP

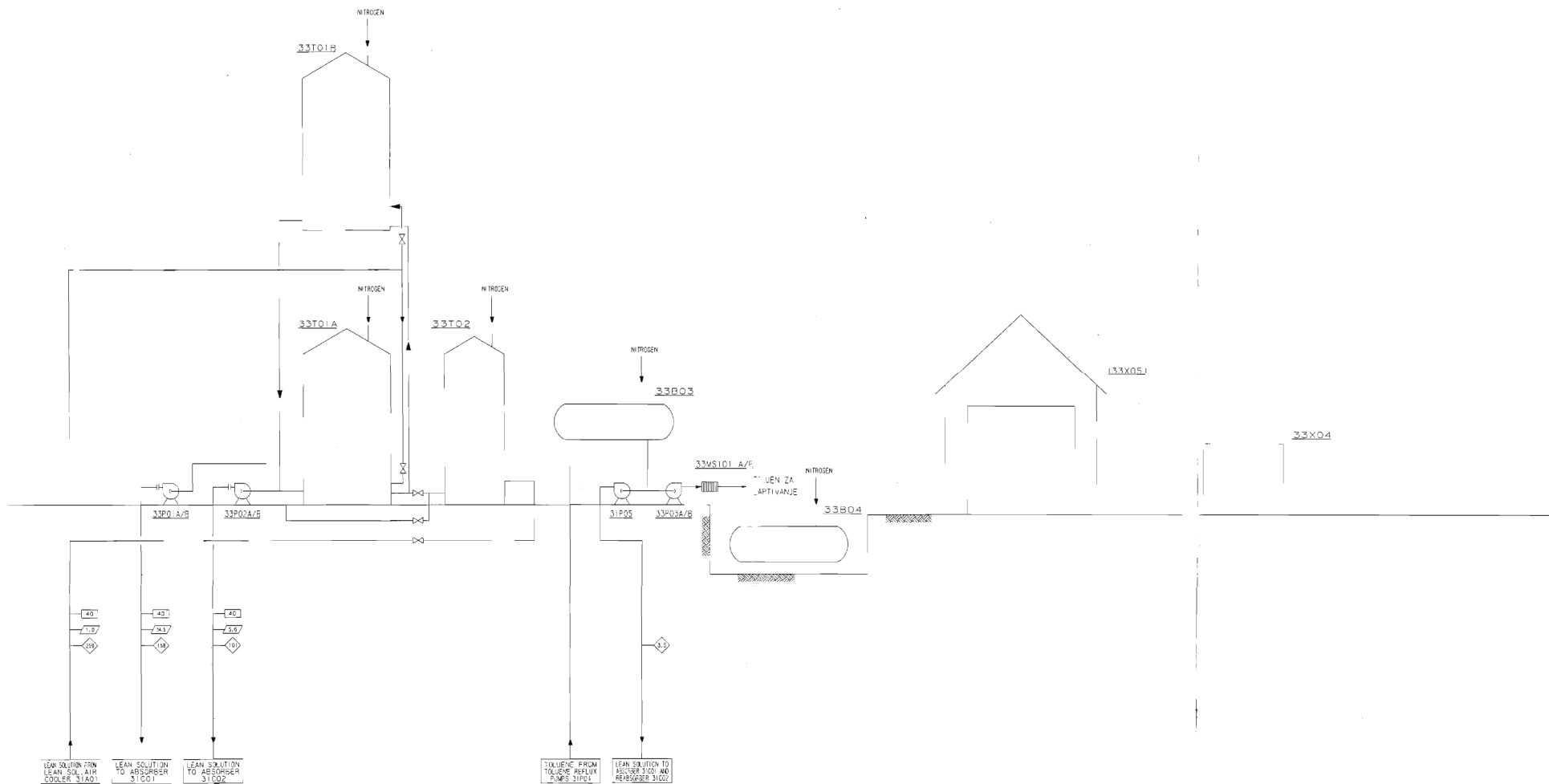
31P05
ABSORBER TOLUENE PUMP

33B04
SLIP

(33X05)
COSORB SOLUTION
PREPARATION UNIT

33X04
REFRIGERATION UNIT

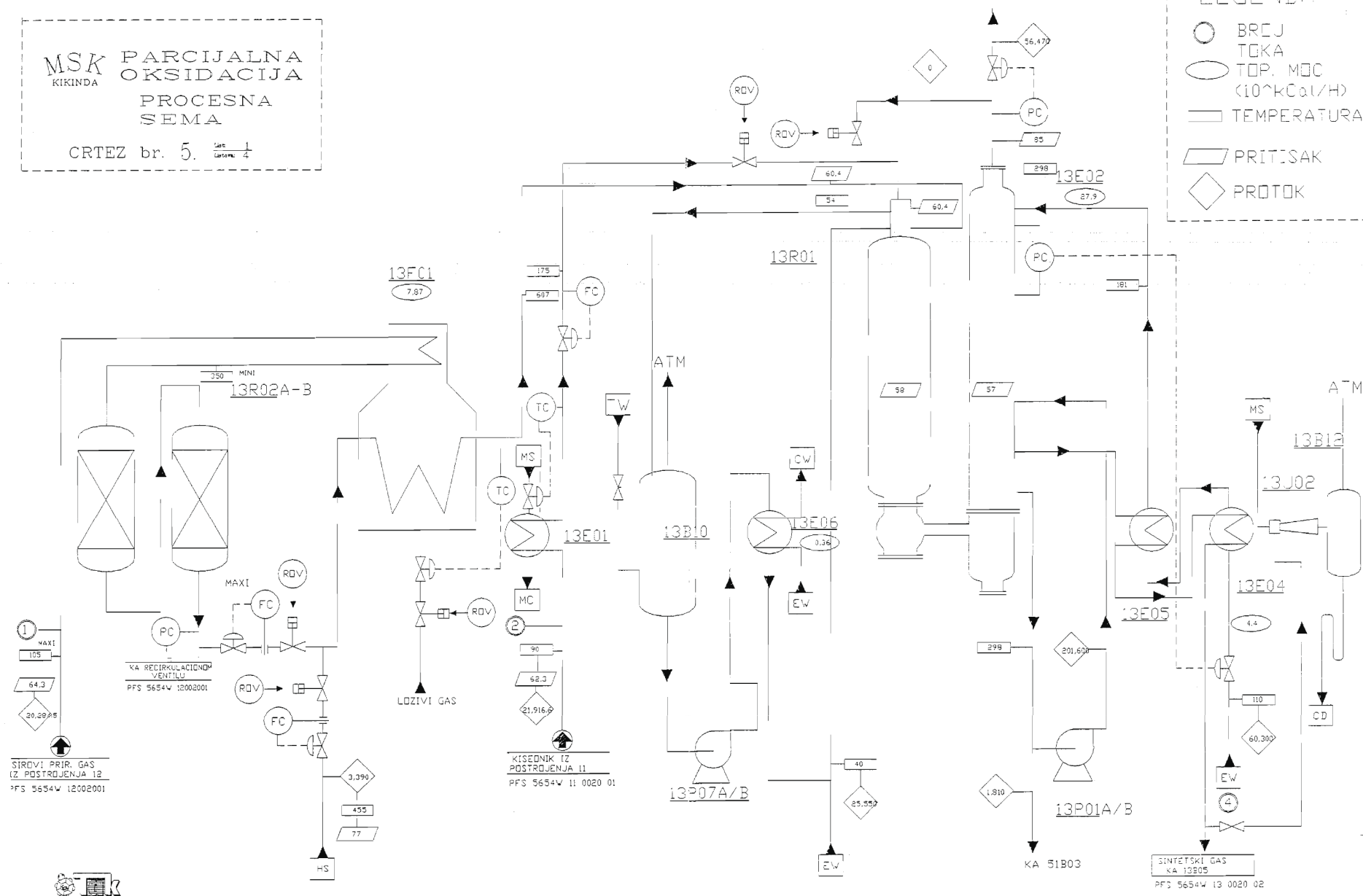
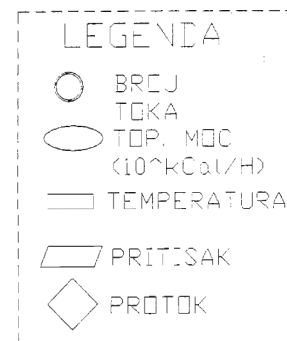
33WS101 A/
TOLUENE TOLUENE
2A LEAN VALVE



MSK		Naslov: PROCESNA SKEMA PROIZVODNJE VODONIKA I UGLJEN MONOKSIDA	
Projekat:		12. IN - INOVISE PLANT PRO. TES SCHEME	
Projekat:	Proj. oznaka: 5654W30002004	MSK štif:	MSK-PS-2121-04
Iskustvo br:	D1	Datum:	02.06.1997.
Prilozak br:	1	Prilozak br:	1
Autor izveštaja:		Overa:	
Miroslav Brankovic		Miroslav Brankovic	
Miroslav Brankovic		Miroslav Brankovic	

MSK PARCIJALNA
KIKINDA OKSIDACIJA
PROCESNA
SEMA

CRTEZ br. 5. Lis: 1
Listova: 4



32E01A/B
PRVI MEDJUFAZNI
HLADNACI

32B01A/B
PRVI MEDJUFAZNI TROSTEPNI KOMPRESORI
SEPARATORI TOULENA UGLJEN MONOKSIDA

32K01A/B

32B02A/B
DRUGI MEDJUFAZNI
SEPARATORI TOULENA

32E02A/B
DRUGI MEDJUFAZNI
HLADNACI

32E09
HLADNACI
UGLEN MONOKSID

32E04
IZMENJIVAC
UGLJEN MONOKSID

32E05
HLADNAC
UGLJEN MONOKSID

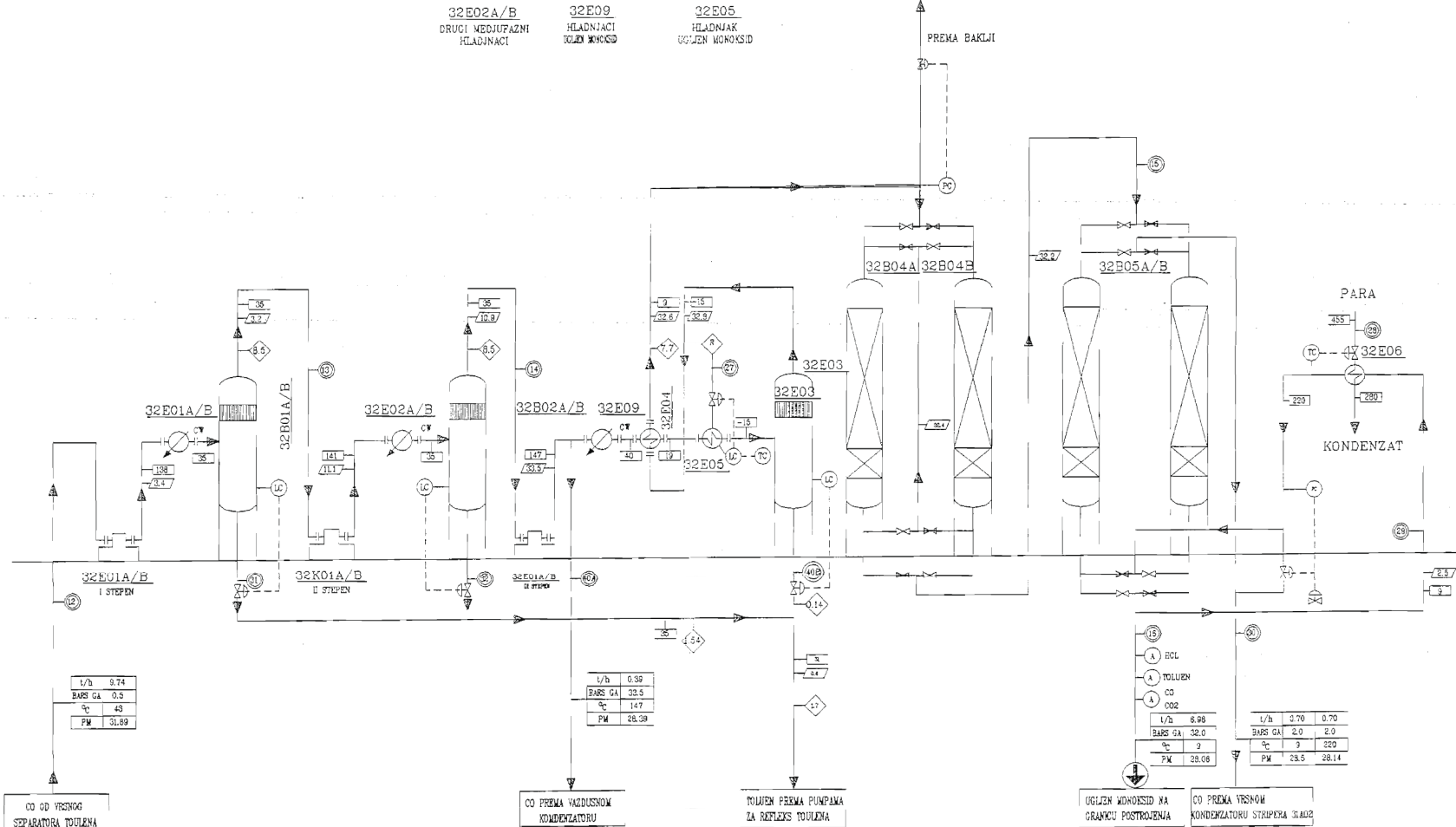
32E03
SEPARATOR TOULENA
TRECEG STEPENA

32B04A/B
OTKLANJANJE HCl
IZ CO-PRODUKTA

PREMA BAKLJI

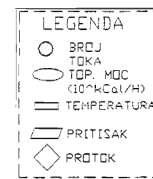
32B05A/B
APSORBACIJA TOULENA
IZ CO-PRODUKTA

32E06
GREJAC ZA REGENERACIJU
GASA IZ CO-PRODUKTA



MSK METANOLSKO SIRCETNI
KOMPLEKS KIKINDA
OBJEKAT POSTROJENJE
UGLJEN MONOKSIDA
CRTEZ PROCESNA
SEMA

32B08A/R
ADSRBER
TOLUENA
I GASA
BOGATOG
VODONIKOM



MSK KIKINDA	METANOSLKO SIRCETNI KOMPLEKS KIKINDA
OBJEKAT	POSTROJENJE UGLJEN MONOKSIDA
CRTEZ	PROCESNA SEMA

MSK05EM

33P01A/B
PUMPE
OSIROMASENE
COSORB
OTOPINE
IZ
ABSORBERA

33P02A/B
PUMPE
OSIROMASENE
COSORB
OTOPINE
IZ
REABSORBERA

33T01
REZERVOAR
COSORB
CIRKULACIJE

33T02
REZERVOAR
PRANJA
TOLENA

33B03
SKLADISNI
REZERVOAR
TOLUENA

33P05
PUMPA
ABSORBERA
TOLUENA

33P03A/B
PUMPE
ZA
ISPIRANJE

33B04
PRIHVATNA
POSUDA

33X04
POSTROJENJE
HLADJENJA

33X04
POSTROJENJE
HLADJENJA

